

# Robotized incubation system for monitoring gases (O<sub>2</sub>, NO, N<sub>2</sub>O N<sub>2</sub>) in denitrifying cultures

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## Abstract

As genomic data for bacteria are unraveled at an increasing speed, there is a need for more efficient and refined techniques to characterize metabolic traits. The regulatory apparatus for denitrification, for instance, has been explored extensively for type strains, but we lack refined observations of how these and wild type denitrifiers respond metabolically to changing environmental conditions. There is a need for new “phenomic” approaches, and the present paper describes one; an automated incubation system for the study of gas kinetics in 15 parallel bacterial cultures. An autosampler with a peristaltic pump takes samples from the headspace, and replaces the sampled gas with He by reversing the pump. The sample flows through the injector of a micro GC (for determination of N<sub>2</sub>, O<sub>2</sub>, CH<sub>4</sub>, CO<sub>2</sub>, N<sub>2</sub>O) to the inlet of a chemoluminescence NO analyzer. The linear range for NO is 0.5–10<sup>4</sup> ppmv (CV=2%, detection limit 0.2 ppmv). The gas leakage of N<sub>2</sub> into the system is low and reproducible, allowing the quantification of N<sub>2</sub> production (in flasks with He+O<sub>2</sub> atmosphere) with a detection limit of 150–200 nmol N<sub>2</sub> for a single time increment. The gas loss by each sampling is taken into account, securing mass balance for all gases, thus allowing accurate estimation of electron flows to the various terminal acceptors (O<sub>2</sub>, NO<sub>2</sub>, NO, N<sub>2</sub>O) throughout the culture’s depletion of O<sub>2</sub> and NO<sub>x</sub>. We present some experimental results with *Agrobacterium tumefaciens*, *Paracoccus denitrificans* and denitrifying communities, demonstrating the system’s potential for unraveling contrasting patterns of denitrification gene expression as a function of concentrations of O<sub>2</sub> and NO in the medium. © 2007 Elsevier B.V. All rights reserved.

**Keywords:** Denitrification; Genome; Phenomic approaches; Robotization

## 1. Introduction

As an increasing number of bacterial genes and whole genomes are being sequenced, the searchable databases for functional and regulatory genes are growing and providing an ever richer basis for data mining. This has fostered an increasing interest in systems biology, i.e. the development of mathematical models to predict phenotypic traits from genomic data. However, phenotypic data are scant, and not organized in databases (with a notable exception for yeasts, [Fernandez-Ricaud et al., 2006](#)), but buried in free text (publications). Rich phenotype/metabolic datasets are recognized as a key element in systems biology approaches ([Kester et al., 1994](#); [Dudley et al., 2005](#); [Van Dien and Schilling, 2006](#)). There is a striking

imbalance between the current advances in genomic information, and the scant amount of phenotype data available.

Denitrification is a good example of the imbalance between genomic and phenomic information. Many functional genes and elements of regulatory networks have been revealed for several type strains ([Baker et al., 1998](#); [Butler and Richardson, 2005](#); [Rodionov et al., 2005](#); [Zumft and Kroneck, 2007](#)), allowing extensive data mining in whole genome databases for identification of regulons and various interconnections between different regulatory systems for N-oxide transformations ([Rodionov et al., 2005](#)). Such genome studies need experimental verification, however; there is a need for more refined comparative physiological experiments on denitrifier gene expression.

In the present paper, we describe a robotized method, which is primarily designed for characterizing denitrifying bacteria (or microbial communities) regarding their gas production/reduction (O<sub>2</sub>, NO, N<sub>2</sub>O and N<sub>2</sub>), hence electron flows to the different

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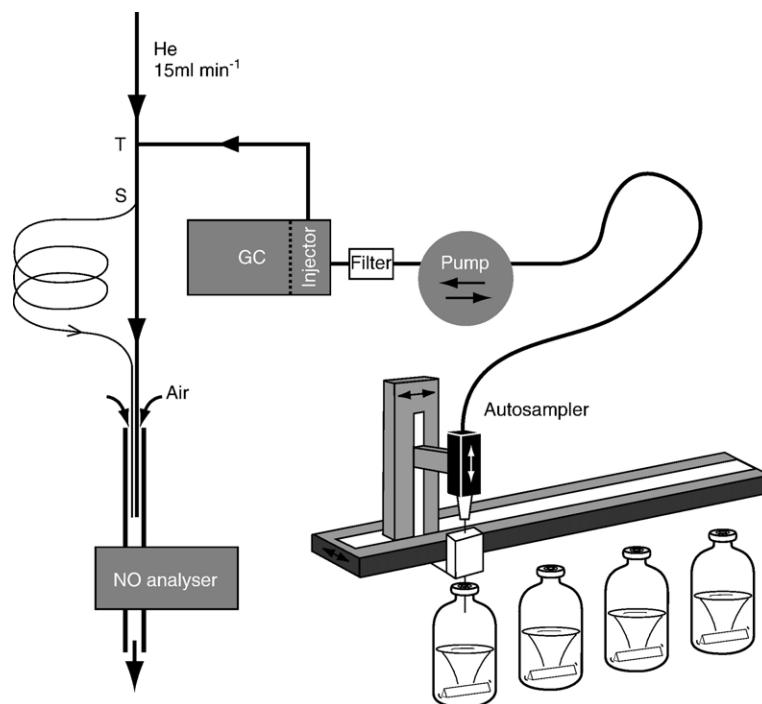


Fig. 1. The sampling and gas analysis system. See text for explanation.

electron acceptors, during and after the transition from oxic to anoxic conditions. Special emphasis has been put on testing the system's ability to monitor the production of  $N_2$  with reasonable precision, thus circumventing the need for using  $^{15}N$  tracer methods or acetylene inhibition of  $N_2O$  reductase. Furthermore, we have developed a sensitive and reliable method to monitor NO and  $O_2$ , which are both master variables for the regulation of denitrification. Diffusion constraints are taken into account, so as to enable a correct estimation of  $O_2$  concentration in the liquid, based on measured  $O_2$  transport from headspace to the liquid phase.

We believe that the data provided by the system will be valuable counterpoints to the increasing amount of information on regulatory networks in denitrifying bacteria. The system provides rich datasets for denitrification under varying conditions. Ultimately, such data can be used to explore the relationship between genotypes and phenotypes of denitrifying bacteria. Our system's ability to monitor NO in combination with other metabolites adds greatly to its value for the study of denitrification as well as other bacterial NO transformations. NO is recognized as a crucial signal molecule (Poole, 2005; Zumft, 2005), an antimicrobial agent produced by macrophages (Spiro, 2007), and possibly an agent in interactions between bacteria (Choi et al., 2006).

The system can also be used to characterize the ability of bacterial communities to express nitrous oxide reductase (nos) during and after the transition from oxic to anoxic conditions, which appears to have major implications for soil emission of  $N_2O$  (Holtan-Hartwig et al., 2002).

The system is described in tedious detail, including various tests of gas leakage and detection capacity. As examples of the system's potentials, we present preliminary data on the kinetics

of  $O_2$ , NO,  $N_2O$  and  $N_2$  production in two type strains, *Paracoccus denitrificans* and *Agrobacterium tumefaciens*, and in a suspension of bacteria extracted from soil by dispersion — density gradient centrifugation.

## 2. Materials and methods

### 2.1. Instrumentation overview

The incubation system is a thermostated water bath (0–40 °C) with positions for 15 crimp-sealed serum flasks (120 ml) with magnetic stirring, plus 3 positions for standards/blanks without stirring. The stirring device is a 15 position submersible magnetic stirrer (Variomag HP 15, art no 41500 from H+P Labortechnik GmbH, Munich Germany) controlled by Variomag Telemodul 40 S (H+P Labortechnik GmbH, Munich, Germany). Alternatively, the system can accommodate 28 serum flasks (120 ml) or 129 small serum flasks (12 ml) without stirring.

Headspace gas is sampled periodically by a Gilson Model 222 (Gilson, leBel, France) autosampler and a Gilson Minipuls 3 peristaltic pump (Fig. 1). The needle is a disposable small-diameter steel needle (0.4 × 40 mm (276 × 11/2), Braun, Braun-Melsungen Germany), guided through a 1 cm long narrow channel (custom made) to avoid bending. To minimize gas leaks, 1/16" steel tubing is used between pump and needle, and between pump and the GC, except for a small piece of Marprene tubing (id=1 mm od=3 mm, part no 902.0016.016, Watson Marlow, England) in the peristaltic pump. Between the pump and the injection system, there is a filter (External sample filter art no 736729, Varian), which protects the injection system of the GC against particles. The filter restricts the gas flow substantially, thus the gas flow is not identical for up- and

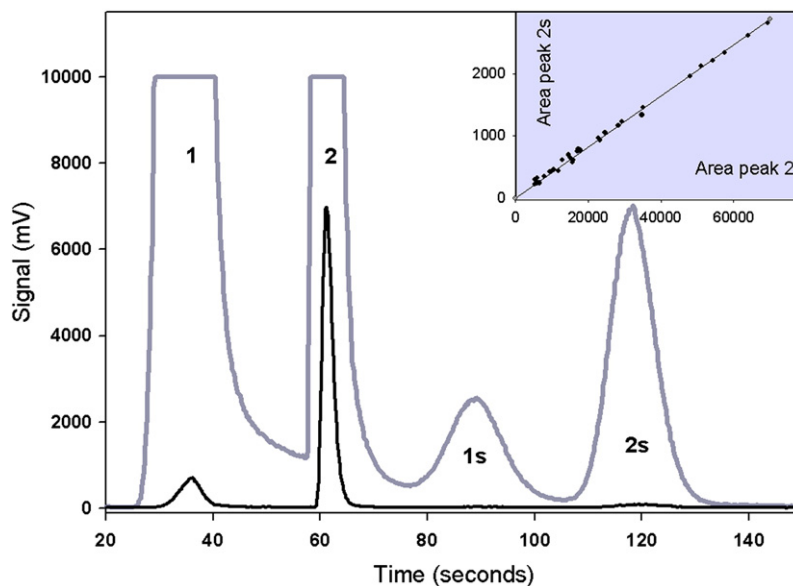


Fig. 2. NO signal peaks from injections of low (black line) and high (grey line) NO concentrations. Peak 1 is the first sample flow which reaches  $T$  (Fig. 1) during peristaltic pumping, peak 2 is the pulse released by the GC-injector immediately after injection. The peaks 1s and 2s are the delayed peaks from the split loop. Inserted figure shows the close linear relationship between peak 2s and 2, for NO-concentrations ranging from the detection limit for peak 2s to the maximum linear range for peak 2. Regression; (area of peak 2s)=0.041\* (area of peak 2),  $r^2=0.99972$ .

down-pumping (the restriction reduce mass flow rate by down-pumping, but not the opposite, since flow rate through the peristaltic pump depends on gas pressure on the inlet side but not on the outlet).

The outlet from the sampling loop of the GC is coupled to a T-piece (T, Fig. 1) with He-flow ( $15 \text{ ml min}^{-1}$ ) which carries the gas further to the open inlet of a chemoluminescence NO-analyzer. The inlet of the NO analyser consists of a 60 cm 1/8''

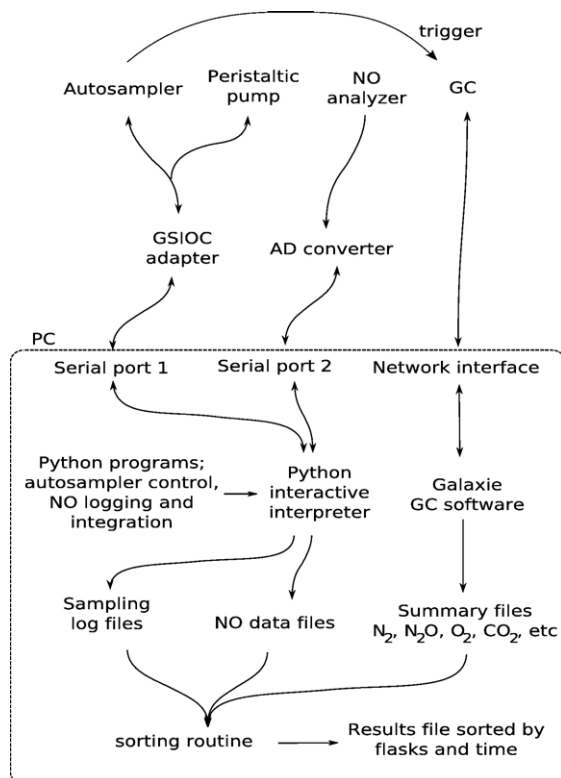


Fig. 3. Overview of instrument controls; signalling, data flows and data filing. See text for explanations.

Table 1  
Parameters for gas solubility in water, based on (Wilhelm et al., 1977); see text for explanation

	$A \text{ cal K}^{-1} \text{ mol}^{-1}$	$B \text{ cal mol}^{-1}$	$C \text{ cal K}^{-1} \text{ mol}^{-1}$	$D \text{ cal K}^{-2} \text{ mol}^{-1}$	Ostwald coefficient*
O <sub>2</sub>	-286.942	15450	36.5593	0.0187662	0.0362
N <sub>2</sub>	-327.85	16757.6	42.84	0.0167645	0.0181
CH <sub>4</sub>	-365.183	18106.7	49.7554	-0.000285033	0.0405
N <sub>2</sub> O	-180.95	13205.8	20.0399	0.0238544	0.785
NO	-333.515	16358.8	45.3253	4.49E-05**	0.0550

Example of calculated gas solubility expressed as L gas per L water at 1 atm partial pressure (Ostwald coefficient) is given in the last column.

\*Solubility in L gas L<sup>-1</sup> water at 1 atm partial pressure, values calculated for 15 °C.

\*\*Estimated by fitting function to reported NO solubilities by the same authors through the temperature range from 273 to 373 K.

tube, which draws air continuously through the instrument (370 ml min<sup>-1</sup>). The He-line has a split (S, Fig. 1) which diverts 4% of the gas through a split loop (SL) consisting of a 60 cm long 0.5 mm id Peek tube followed by a 120 cm long 1.5 mm id PTFE tube. Both the main He-line (carrying 96% of the sample) and the split loop end approximately 30 cm inside the inlet tube of the NO-analyzer. The He-flow rate by the T-piece is 15 ml/min, which greatly exceeds the flow rate of the sampling pump, thus hindering air from entering the incubation vials when reversing the pump (by down-pumping to replace sampled gas).

The design of the sample transfer to the chemoluminescence NO analyzer represents a simple solution for analysing NO in small gas samples, compared to that proposed by (Kester et al., 1994). The split loop secures a high linear range for the NO detection. Since the fraction (4%) of the sample flowing through the split loop arrives 60 s later than the main pulse, it appears as a separate peak which is broader than the main peak (peak 2 s versus peak 2, Fig. 2). The side loop thus increases the linear range with a factor of 100 (not 25, since the peak is broader than the main pulse peak). Two typical NO response curves are shown in Fig. 2, one with NO concentrations exceeding the

linear range for the main pulse. The absolute detection limit for NO with our injection system is 0.2 ppm (=3 times coefficient of variation for injections from He filled blanks). Linear response was achieved from 0.5 ppmv.

The autosampler and the peristaltic pump are controlled by the computer. The injection program secures that the needle pierces the septa at different places each time, thus minimizing the risk of mechanical leaks. The program also controls the direction, speed and timing of the pumping. By carefully measuring flow rate for up- and down pumping (which will not be equal due to restriction by the gas filter), one can secure that sampled gas is replaced by an equal volume of He. The timing of the pumping can be set so as to ensure that the returned gas volume slightly exceeds the sampled volume (as measured with 1 atmosphere pressure at the needle tip). This results in a build up of a slight overpressure in the incubation flasks (reaching a stable level after a few samplings because the gas flow rate during pumping up from the flask will increase with increasing gas pressure in the flask).

## 2.2. Analytical instruments

The GC is a Varian CP4900 microGC equipped with two columns (10 m poraPLOT U and 20 m 5 Å Molsieve), with separate injectors and TCD detectors. The GC's own sampling pumps are uncoupled (the system uses the external peristaltic pump), and the system is operated with open injectors (i.e. the sample flow through the two injectors is controlled by the peristaltic pump): The injection time on both columns are 50 ms, column pressure (He) and temperature are 200 kPa and 36 °C for the PLOT U column, and 250 kPa and 50 °C for the Molsieve column.

The NO analyser is a Chemoluminescence NOx analyser Model 200A (Advanced Pollution Instrumentation, San Diego, USA), measuring NO at high frequency, (20 Hz; NO<sub>2</sub>-option disabled, thus NO-signal is recorded continuously). The NO signal is digitalized and the peaks are integrated by a Python

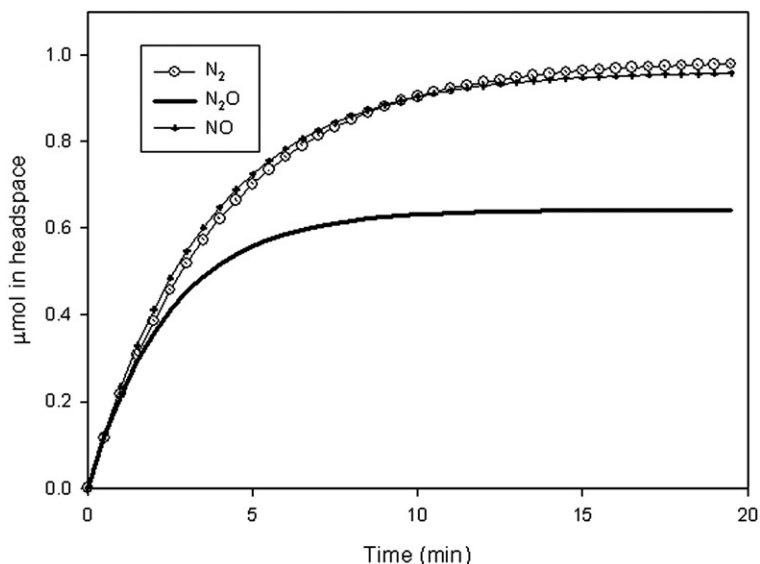


Fig. 4. Calculated gas transport from liquid to headspace for a pulse of 1 mol of N<sub>2</sub>, N<sub>2</sub>O and NO (temperature 15 °C, volume of water 50 ml, total volume 120 ml).

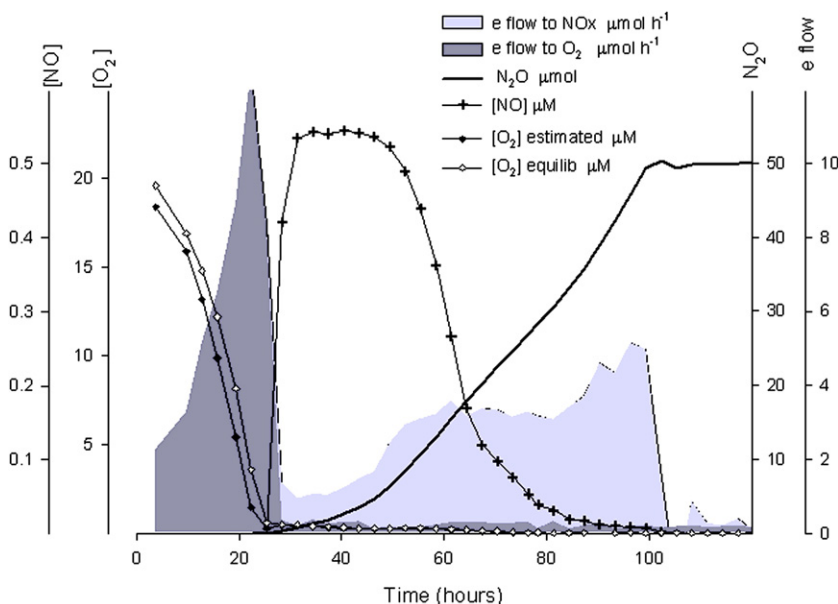


Fig. 5. Gas kinetics and electron flows in *Agrobacterium tumefaciens* during transition from oxic to anoxic conditions. Cells grown in 50 ml Siström's medium with 1 mM KNO<sub>3</sub> at 15 °C and initially 1.4 vol% O<sub>2</sub> in headspace. Two O<sub>2</sub> concentrations in the liquid are shown; the estimated concentration as calculated from observed transport rate ([O<sub>2</sub>] estimated), and the concentration if in equilibrium with each measurement of O<sub>2</sub> in headspace ([O<sub>2</sub>] equilib). [NO] is the NO concentrations in the liquid (μM), N<sub>2</sub>O is μmol N<sub>2</sub>O flask<sup>-1</sup> (losses by sampling are added). Electron flow to O<sub>2</sub> and to NO<sub>x</sub>, in μmol flask<sup>-1</sup> h<sup>-1</sup> are shown as shaded areas. The data stem from a larger series of incubations by L Bergaust et al., Norwegian University of Life Sciences (manuscript in preparation).

program. Calibration is routinely done by injecting known standards (25 ppm NO in N<sub>2</sub>). The present split system secures a linear response over the range 0.5–10<sup>4</sup> ppmv, and the detection limit is approximately 0.25 ppmv (much higher than the detection limit for the instrument, due to dilution).

### 2.3. Connections, system control and datalogging

Fig. 3 shows an overview of the connections, signalling and data filing of the system. The computer is connected to the autosampler through one of the PC's serial ports (RS232, using a GSIOC cable and adapter from Gilson). The connection with the micro-GC is through a network interface. There is also a cable going from the relay output of the autosampler to an input channel of the GC (trigger, Fig. 3). This cable is used for triggering the GC injector. Another serial port of the PC is used for reading the AD converter connected to the analogue output of the NO analyzer (reading frequency 5 Hz).

The program controlling the autosampler and reading the AD converter is written in the Python programming language, and is normally run from the interactive Python shell. This enables easy debugging and testing (all functions for controlling the pump and autosampler are available at the command prompt).

When a sample is taken, the Python program directs the autosampler and pump to take a sample from a given flask position, and then to trigger the GC injector. The logging of the AD converter from the NO analyzer starts just before the pump starts pumping gas from the flask, and runs in a separate thread in Python. The separate thread is used to allow for the logging to run while the sampling procedure continues.

For each sample taken, the Python program writes a line of text to a log file (the sampling log file). The line of text consists of the time of sampling (triggering time) and an identifier of the flask sampled (i.e. flask position in the rack). The GC data acquisition software (Galaxie, <http://www.varianinc.com>) provides summary files for all gas peaks except NO-peaks, which are stored by the Python program in separate files (one for each sample). The time of sampling can be found both in the output files of Galaxie and in the NO data files, as well as in the sampling log file written by the Python program. These files are used by a sorting routine which links each chromatogram to a flask and sorts the measurements before presenting them in a spreadsheet.

The control of the pump and the autosampler allows the system to minimize leaks of N<sub>2</sub> and O<sub>2</sub> into the flasks by the sampling, firstly by pumping down (i.e. He-flow through the system, see Fig. 1) continuously between each sampling, secondly by never piercing the septum in the same place twice (using a Halton sequence for piercing within a predefined circle of the septum).

### 2.4. He washing

A prerequisite for measuring N<sub>2</sub> production is to secure initial low concentrations of N<sub>2</sub>. This is done by repeated cycles of evacuation and He-filling. A He-line and a vacuum line are connected via computer-controlled valves to a manifold with 15 flexible steel tubes with Luer fitting for needles at the end. Sterility is secured by mounting 0.2 μm pore size filters between the steel tube and the needle. The needles pierce the septa of the flasks, which are then repeatedly evacuated and filled with He while stirred vigorously (180 s evacuation, 30 s filling with He to 1.5 atm, 6 repeated cycles). The overpressure of He is

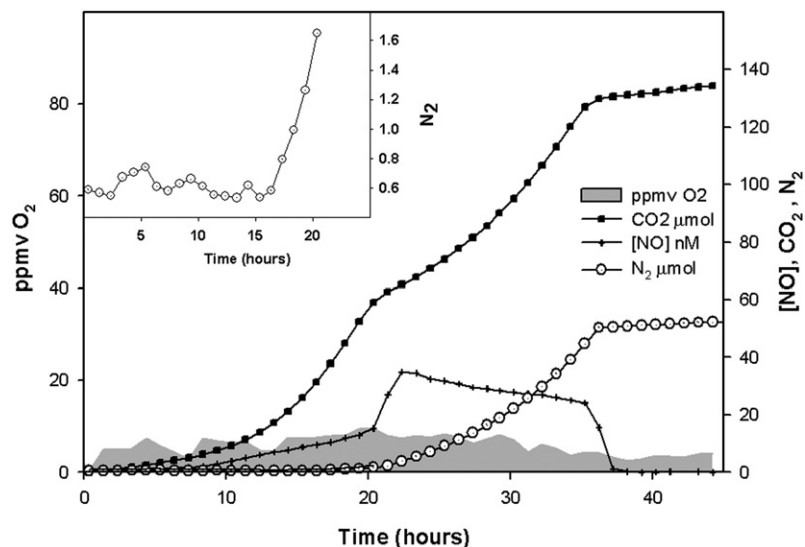


Fig. 6. Incubation experiment with *Paracoccus denitrificans* grown in 50 ml Siströms medium (C source, succinate) with 2 mM  $\text{KNO}_3$  at 15 °C and initially near zero  $\text{O}_2$  in headspace (He atmosphere).  $\text{CO}_2$  and  $\text{N}_2$  are shown as  $\mu\text{mol flask}^{-1}$ . The NO concentrations in the medium [NO] is given as nM. Uncertain estimates of low  $\text{O}_2$  concentrations are illustrated by the shaded area (ppmv  $\text{O}_2$  in headspace, left axis). Inserted figure shows  $\text{N}_2$  ( $\mu\text{mol flask}^{-1}$ ) during the first 20 h. The data stem from a series of incubations by Bergaust et al., Norwegian University of Life Sciences (manuscript in preparation).

released through a syringe filled with water (no piston) to prevent air entry, and the desired volume of pure  $\text{O}_2$  is added by a gastight syringe (and overpressure is released again). He-washing (and subsequent injection of  $\text{O}_2$ ) is routinely done prior to inoculation, to avoid exposure of the inoculum to the anoxic conditions created during He washing.

### 2.5. Developments and performance testing

Preliminary tests showed that care is needed to avoid gas leaks between the glass and the rubber septa (Brown Crimp seals with rubber septa Cat no 151290, and Macherey-Nagel Rubber stoppers N20 Art no 702-931). A thin film of vacuum grease (Glisseal silicone-free vacuum grease, Borer Chemie AG, Switzerland) and brute force when tightening the crimp seals eliminated such leaks. Gas diffusion through the septa was tested by analysing 7 flasks 24 h after He-washing and then after 40 days storage in air at room temperature.

Each sampling will inevitably result in small inputs of both  $\text{N}_2$  and  $\text{O}_2$  due to diffusion through the Marprene tubing, the membranes in GC injector, and connections. These inputs were quantified by repeated sampling from flasks filled with He (1 atm.). These gas inputs could be reduced further by enclosing the peristaltic pump in a He-filled chamber (see results), but this was not adopted as a routine.

Other sources of  $\text{N}_2$  inputs to the headspace, such as gradual release of  $\text{N}_2$  which was not removed by the He-washing (i.e.  $\text{N}_2$  remaining in water, the rubber septa and the Teflon cover of the stirring bars), were investigated by monitoring gas concentrations during the first 48 h after He-washing of flasks containing 50 ml sterile water.

Each sampling involves a dilution of the headspace (the sampled gas is replaced with He), which needs to be known to ensure correct mass balance. This dilution was quantified by 25 repeated samplings of 4 flasks (120 ml) initially filled with air.

The dilution has also been routinely measured in every subsequent experiment, by including standard flasks with known initial gas concentrations.

When analysing different cultures which produce widely different concentrations of NO or  $\text{N}_2\text{O}$ , the carry over from one culture to the next is a potential problem. We tested this by running a sequence of flasks where every second flask contained pure He, and the others various standard gas mixtures (25 ppmv NO in  $\text{N}_2$ , 150 ppmv  $\text{N}_2\text{O}$  and 1%  $\text{CO}_2$  in He, 21%  $\text{O}_2$  in  $\text{N}_2$ ).

The precision of the gas analyses were evaluated by 20 repeated analyses from a series of single flasks. The measured concentrations, corrected for the known dilution by sampling, were used to estimate the coefficient of variation (CV). Since this was expected to be concentration dependent, the experiment was conducted with a series of flasks with widely different initial concentrations of the gases in question (NO,  $\text{N}_2\text{O}$ ,  $\text{N}_2$ ,  $\text{O}_2$ ).

The rate of gas transport in/out of the liquid phase is an important characteristic of the system, which needs to be known for a correct calculation of the  $\text{O}_2$  concentrations in the liquid. The concentration of dissolved  $\text{O}_2$  can be calculated as a function of observed headspace concentrations and transport rates from the headspace to liquid. The transport coefficient cannot be calculated from standard diffusion coefficients since it depends on turbulence and rippling of the liquid surface by the stirring. Hence the transport rate coefficient is system specific (depending on liquid volume per flask, speed of stirring, and temperature), and must be determined experimentally. This was done for a standard condition most frequently used in our lab: 50 ml liquid, 15 °C and maximum stirring speed (=800 rpm). First, 50 ml distilled water was equilibrated to 1 atm pure  $\text{O}_2$  in the headspace. This  $\text{O}_2$  was then removed by purging the headspace with He (two needles through the septum, rapid He-flow, no evacuation and no stirring during purging), and the  $\text{O}_2$  diffusion into the headspace was then monitored during normal stirring until it approached equilibrium.

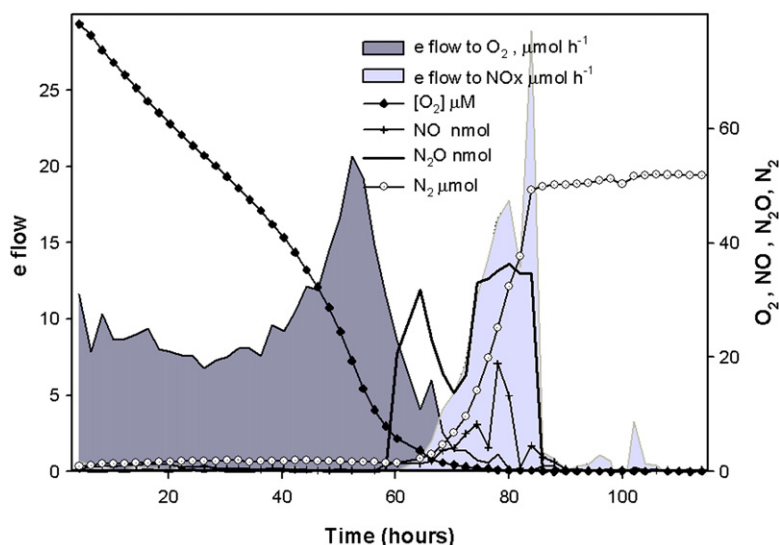


Fig. 7. O<sub>2</sub> depletion and denitrification by suspension of soil bacteria (extracted by dispersion and density gradient centrifugation), incubated in 50 ml mineral salt medium with vitamins, glucose (1 g L<sup>-1</sup>), HEPES buffer (31 mM, pH=7), 2 mM NO<sub>3</sub><sup>-</sup> and 0.1 mM NO<sub>2</sub><sup>-</sup>. The line graphs show the estimated O<sub>2</sub> concentration in the liquid ([O<sub>2</sub>] μM), and the amounts of NO (nmol), N<sub>2</sub>O (nmol) and N<sub>2</sub> (μmol) in the whole flask (N<sub>2</sub> includes that lost by sampling). The shaded areas shows calculated electron flow to O<sub>2</sub> and NO<sub>x</sub> in each time increment. Data stem from a series of incubations by Nicholas Morley et al., Norwegian University of Life Sciences and University of Aberdeen, UK (manuscript in preparation).

Correct estimates of gas production/reduction rates depend on the solubility of each gas. Our calculation of gas solubility for NO, N<sub>2</sub>O, N<sub>2</sub> and O<sub>2</sub>, are based on Wilhelm et al. (1977), calculating the mole fraction (mol gas per mol water) of each gas as  $X_2 = e^{(A+B/T+C \cdot \ln(T)+D \cdot T)/R}$ , where  $T$  is temperature (K),  $R$  is 1.9872 cal mol<sup>-1</sup> K<sup>-1</sup>;  $A$ ,  $B$ ,  $C$ , and  $D$  are parameters (individual values for each gas) given in Table 1. We identified an error in Wilhelm et al. (1977); the parameter  $D$  for NO should be  $4.493 \cdot 10^{-5}$  cal K<sup>-2</sup> mol<sup>-1</sup>, for the function to comply with NO solubilities reported by the same authors. Equilibrium concentrations of CO<sub>2</sub> and carbonates are calculated as a function of temperature ( $T$ , °K) and pH, according to Stumm and Morgan (1996).

Performance of the system is exemplified by selected data from O<sub>2</sub> depletion experiments with *A. tumefaciens* (which lacks N<sub>2</sub>O reductase), *P. denitrificans*, and suspensions of soil bacteria extracted from soil by density gradient centrifugation (Aakra et al., 2000).

### 3. Results

#### 3.1. Gas leaks

The measured leak rate through the septum during the 40 days storage ranged from 13 to 30 nmol N<sub>2</sub> day<sup>-1</sup> and from 10 to 24 nmol O<sub>2</sub> day<sup>-1</sup>. The similar leak rates for N<sub>2</sub> and O<sub>2</sub> suggest that the leakage is primarily by diffusion through the septum rubber (not through open channels), since there is normally a 3–4:1 ratio between diffusion coefficient for O<sub>2</sub> versus that of N<sub>2</sub> in polymers (Haraya and Hwang, 1992; Polotskaya et al., 1999). Higher leak rates (and with N<sub>2</sub>:O<sub>2</sub> ratios closer to that in the atmosphere) have been encountered when septa were pierced by a partly damaged needle.

The injection system is a more serious source for O<sub>2</sub> and N<sub>2</sub> contamination (carried with the He-flow when pumping down).

By pumping He through the system (pumping down) when idle (i.e. between each sampling), the diffusion of N<sub>2</sub> and O<sub>2</sub> into the needle was minimized. Nevertheless, the average contamination by sampling was found to be 61 nmol N<sub>2</sub> (ranging from 53 to 73) and 22 nmol O<sub>2</sub> (range 19–24) per injection. Enclosing the pump in a He-filled chamber lowered the leak to approximately 21 nmol N<sub>2</sub> and 12 nmol O<sub>2</sub> per injection. Such He-enclosure is costly and time consuming to sustain, however, and has not been adopted as a routine. But the experiment helped to identify the peristaltic pump as the main source of N<sub>2</sub> and O<sub>2</sub> leaks into the system. In subsequent incubation experiments, we found the contamination through the injection system is consistently low, but somewhat variable (range 60–120 nmol N<sub>2</sub>, 20–50 nmol O<sub>2</sub> per injection), possibly depending on variable leaks in the connections between steel tubing and the rubber tube. As a consequence, control flasks with He are included in every incubation experiment where N<sub>2</sub> production is to be quantified.

Another source of contamination is the release of N<sub>2</sub> and O<sub>2</sub> which remain absorbed in the rubber septa and Teflon cover of the magnetic bar after a standard He wash procedure. Immediately after a He-wash, this emission was 150–200 nmol N<sub>2</sub> and 50 nmol O<sub>2</sub> h<sup>-1</sup> and gradually declined to reach very low rates after 10–15 h. Standard procedure is thus to He-wash the flasks at least one day before inoculation, to secure a stable background of O<sub>2</sub> and N<sub>2</sub> before inoculation.

#### 3.2. Memory effects, dilution by sampling, and precision

When analysing different cultures which produce widely different concentrations of NO or N<sub>2</sub>O, the carry over from one culture to the next is a potential problem. As programmed, however, the injection system is efficiently cleaned between each sampling by the pumping of He through the system during

the entire chromatogram of each sample (180 s). The measured carry over was found to be less than 0.1%.

The sample gas flow during pumping from the flasks is  $8.2 \text{ ml min}^{-1}$ . It was found necessary to pump for 30 s to ensure that sample gas reached the T-piece (seen as a rising NO signal, Fig. 2), thus 4.2 ml is withdrawn from the flask for each sampling. The gas flow when pumping down (after the injection by the GC) is 10% lower due to the restriction by the filter between the pump and the GC, and the down-pumping was thus prolonged to 33.4 s to maintain 1 atmosphere after sampling. The dilution of the headspace gas by each sampling (as measured by repeated samplings of 120 ml flasks filled with air) was 1.6% throughout the entire sampling series, equivalent to 1.9 ml gas replaced by He for each sampling. Thus, a substantial fraction of the sampled headspace gas was returned to the flask by the down-pumping after GC-injection. Control flasks (no bacteria) are routinely included in experiments to calibrate the GC as well as to assess the dilution. The dilution rate appears to vary somewhat between experiments (but is constant within each), possibly depending on variable tightening of the peristaltic pump.

The precision of the gas analyses as evaluated by 20 repeated analyses from single flasks (corrected for the dilution by sampling), demonstrated a low but concentration-dependent variability. For high concentrations of  $\text{N}_2$  and  $\text{O}_2$  (10,000 ppmv) and  $\text{N}_2\text{O}$  (150 ppmv), the coefficients of variation (CV) were 0.4–0.5%. For concentrations much below ambient, the CV was somewhat higher: 1.3% for  $\text{O}_2$  at 800 ppm, and 0.7% for  $\text{N}_2$  at 2500 ppmv. For NO, the standard deviation was approximately 2% (determined for a 25 ppmv NO-standard diluted to 5 ppmv in He). Measurements of very low concentrations of  $\text{O}_2$  and  $\text{N}_2$  (10–50 ppmv) were more variable, since they are affected by minor but variable air contamination during pumping.

The absolute detection limit for  $\text{N}_2$  production during a single time increment (between two samplings) was evaluated based on  $\text{N}_2$  data from sterile control flasks. The calculated  $\Delta\text{N}_2$  for 20 increments, defined as the apparent changes in  $\text{N}_2$  for each increment (after correcting for the dilution and leak per injection), had an average close to zero ( $-2.5 \text{ nmol N flask}^{-1} \text{ injection}^{-1}$ ) and a standard deviation of  $54 \text{ nmol N}_2 \text{ flask}^{-1}$ . This would imply that the detection limit for  $\text{N}_2$  production in a single increment is  $160 \text{ nmol N}_2 \text{ flask}^{-1} \text{ injection}^{-1}$  (=3 times the standard deviation).

### 3.3. Diffusion rates between liquid and headspace

In theory, the  $\text{O}_2$  transport between the liquid phase and the headspace is a function of the concentrations in the two phases,  $\text{O}_2$  solubility, and a coefficient for transport of  $\text{O}_2$  between the liquid and the headspace:

$$\text{Transport between liquid and headspace} \quad (1)$$

$$V = k_t(k_H P_{\text{O}_2} - [\text{O}_2])$$

Where

- $-V$  is the transport rate ( $\text{mol O}_2 \text{ s}^{-1}$ )
- $-k_t$  is the coefficient for transport from gas to liquid ( $\text{L s}^{-1}$ )
- $-P_{\text{O}_2}$  is  $\text{O}_2$  partial pressure in headspace (atm)

- $-k_H$  is the solubility of  $\text{O}_2$  in water ( $\text{mol L}^{-1} \text{ atm}^{-1}$ )
- $-[\text{O}_2]$  is  $\text{O}_2$  concentration in the liquid ( $\text{mol L}^{-1}$ )

Measured  $\text{O}_2$  transport from  $\text{O}_2$ -saturated distilled water to a He-flushed headspace (see Materials and methods section) was used to estimate  $k_t$ . We ran 4 independent experiments at  $20^\circ\text{C}$ , with 50 ml distilled water per flask, measuring  $\text{O}_2$  accumulation in the headspace every 210 s over a period of 1050 s after starting the stirring. The model (i.e. Eq. (1) plus the known dilution of the headspace by each sampling) was fitted to the data, and yielded  $K_t$  values ranging from 2.7 to  $2.8 \cdot 10^{-4} \text{ L s}^{-1}$ .

Solving Eq. (1) for  $[\text{O}_2]$  gives  $[\text{O}_2] = k_H P_{\text{O}_2} - V/k_t$ , which can be used to calculate average  $\text{O}_2$  concentration in the liquid for each time increment between two samplings (estimating  $V$  by the difference between measured  $P_{\text{O}_2}$  in the first sample (corrected for the dilution by the same sampling) and the measured  $P_{\text{O}_2}$  in the subsequent sample).

The transport coefficient can also be used to evaluate the time it takes to reach equilibrium between liquid and headspace for the other gases produced in the liquid. The transport rate of a gas to the headspace,  $dn/dt$  is given by the equation for  $V$  above (Eq. (1)). When integrated, Eq. (1) gives

$$n(t) = (n(0) - b/a)e^{-at} + b/a \quad (2)$$

where

$$a = k_t(k_H RT/V_g + 1/V_w) \quad (3)$$

and

$$b = k_t n_{\text{tot}}/V_w \quad (4)$$

Here,  $n(t)$  is the amount of gas in headspace (mol),  $n(0)$  is the initial amount of gas in headspace,  $n_{\text{tot}}$  is the total amount of gas,  $R$  is the gas constant ( $0.082 \text{ L atm K}^{-1} \text{ mol}^{-1}$ ),  $T$  is temperature (K),  $V_g$  is the volume of liquid (L),  $V_w$  is the volume of water (L),  $k_H$  is the solubility and  $k_t$  is the transport coefficient.

We can assume that the transport coefficients ( $k_t$ ) for the other gases than  $\text{O}_2$  can be estimated as  $k_t D_g/D_{\text{O}_2}$ , where  $D_{\text{O}_2}$  and  $D_g$  are diffusion coefficients (in water) for  $\text{O}_2$  and the gas in question, respectively, and  $k_t$  is the system specific transport coefficient for  $\text{O}_2$ . The diffusion coefficients at  $15^\circ\text{C}$  are; 1.67, 1.62, 1.67 and  $1.52 (\cdot 10^{-5} \text{ cm}^2 \text{ s}^{-1})$  for  $\text{O}_2$ ,  $\text{N}_2\text{O}$ , NO, and  $\text{N}_2$ , respectively (data from Lide (2005) and Zacharia and Deen (2005); the Wilke-Chang correction (Wilke and Chang, 1955) was used to obtain D for  $\text{N}_2$  and NO).

Assume that the bacteria emit a pulse of  $1 \mu\text{mol}$  of NO,  $\text{N}_2\text{O}$  or  $\text{N}_2$  in a flask with zero concentration of the gas in headspace, i.e.  $n_{\text{tot}} = 1 \mu\text{mol}$  and  $n_0 = 0$ . The curves for  $n(t)$  for the three gases are shown in Fig. 4.

### 3.4. Denitrification experiments, mass balances and kinetics

Fig. 5 shows an experiment with *A. tumefaciens* grown in Siström's medium (Lueking et al., 1978) containing 1 mM  $\text{KNO}_3$ . The culture was allowed to deplete  $\text{O}_2$  by its own respiration. The estimated  $\text{O}_2$  concentrations in the liquid



medium ( $[O_2]$  estimated; in this case the plotted values are the average of the two encompassing time increments) are only slightly below the equilibrium concentrations ( $[O_2]$  equil., i.e. the concentration if in equilibrium with measured  $P_{O_2}$  in headspace) during the entire oxic phase. NO accumulated to 500 nM in the liquid (220 ppmv in the headspace). The  $N_2O$  reached a stable plateau (as  $NO_3$  was depleted, not shown) at  $24.7 \mu\text{mol } N_2O = 49.4 \mu\text{mol } N_2O-N$  per flask (NB; these values include losses by sampling dilution), which is 98.8% of the initial amount of  $NO_3-N$  ( $=50 \mu\text{mol}$  per flask). There was no detectable  $N_2$  production (not shown), confirming that *A. tumefaciens* lacks nitrous oxide reductase. Similar recoveries ( $\pm 5\%$ ) of added nitrate – or nitrite – N (as  $N_2O$ ) have been observed in 50 equivalent incubations with *A. tumefaciens* under varying conditions.

Fig. 5 also illustrates the electron flow rate to  $O_2$  and to  $NO_x$ ; the latter is based on observed equilibrium  $NO_2^-$  concentrations at 20–40  $\mu\text{M}$  ( $=1-2 \mu\text{mol/flask}$ ) during the entire period with active denitrification (not shown). The transition from  $O_2$  respiration to denitrification is seen to represent a severe reduction in energy flow for *A. tumefaciens*.

Fig. 6 is an example of the experiments conducted with *P. denitrificans* grown in 50 ml Sistrom's medium (C source, succinate), buffered with 20 mM phosphate, initial pH=6.5, and initial  $O_2$  concentration near zero. The final  $N_2$  plateau (which includes that lost by sampling) was  $52 \mu\text{mol}$  per flask, which is 104% of the  $NO_3-N$  of the medium. The NO concentration plateau during active denitrification is one order of magnitude lower than for *Agrobacterium*. In this particular pH treatment,  $N_2O$  was not detected (but was at lower pH levels). The detection limit for  $N_2O$  (0.5 ppmv) is equivalent to 2.5 nmol per flask. The  $CO_2$  accumulation appears to slow down after 20 h, coinciding with the sharp increase in NO and  $N_2$  accumulation. This is most probably an artefact, however, caused by the inevitable alkalisation of the medium by denitrification (the  $CO_2$  accumulation was calculated assuming constant pH=6.5). This illustrates the limited value of measuring  $CO_2$ , unless pH is carefully monitored. The insert in Fig. 6 shows the  $N_2$  data in detail for the first 20 h, which strongly suggest a significant  $N_2$ -production starting at least 5 h before the sharp rise in NO. Prior to that (15–17 h), any  $N_2$  production is below the detection limit for the system (which is  $150-200 \text{ nmol flask}^{-1} \text{ h}^{-1}$ ).

To illustrate the problem with determination of low levels of  $O_2$ , we have included the measured concentrations (ppmv in headspace) as a shaded area. The variable but low  $O_2$  concentrations prove that *Paracoccus* is actively respiring  $O_2$  during the entire period of denitrification, consuming practically all the  $O_2$  which leaks into the system due to sampling ( $19-25 \text{ nmol } O_2 \text{ flask}^{-1} \text{ sampling}^{-1}$ , equivalent to 6–8 ppmv  $O_2 \text{ sampling}^{-1}$ ).

Fig. 7 shows an example from a series of experiments where bacteria were extracted from soil by dispersion density gradient centrifugation and then incubated under different conditions (Nick Morley et al., unpublished). The experimental conditions are given in the figure legend. As for the other experiments, there is a good (96%) recovery of added  $NO_3^- + NO_2^-$  as  $N_2$ . The NO levels are comparable to those in *Paracoccus* (1 nmol/flask

is equivalent to 0.76 nM in the liquid). Denitrification starts before  $O_2$  is depleted, and is first detected as an increase in NO and  $N_2O$  (after 58 h), and then as  $N_2$  (after 64 h). The apparent lag in  $N_2$  accumulation could be taken to suggest that the expression of  $N_2O$  reductase lags behind that of  $NO_2^-$  and NO reductase. This is uncertain, however, since the detection limit for  $N_2$  production is approximately two orders of magnitude higher than that for NO and  $N_2O$  (not due to lower instrument sensitivity, but due to variable contamination by atmospheric  $N_2$  in the sampling apparatus, see previous discussion).

#### 4. Discussion

We have described the system in detail to provide a basis for the construction of similar systems by others. For the same reason, we have described a variety of tests, and demonstrated its potentials as well as limitations. Numerous details are important for making a robot of this kind, and to run successful experiments with it. It is far from trivial to measure the kinetics of  $N_2$  production by denitrification without isotopes or inhibitors. Neither is it trivial to measure NO kinetics in bacterial cultures, or to run batch experiments with proper mass balance for gases despite frequent sampling from headspace. We believe, that this kind of instrumentation can generate valuable information for a number of purposes, and foresee the construction of similar robots elsewhere. All the components are commercially available, except for the custom made racks, the needle guide on the autosampler, and the various programs controlling the instruments, signal integration, filing and sorting the data.

The experimental results presented are examples from ongoing studies with denitrification, and demonstrates some of the potentials of the system. The measured coefficient of gas transport between headspace and liquid (Fig. 4) implies that near steady state conditions can be assumed for all gases other than  $O_2$ , except during periods with abrupt changes in gas production/consumption. Rapid NO oscillations, as observed by mass spectrometry with direct membrane inlet from cultures of *P. denitrificans* (Kunak et al., 2004; Spiro, 2007), would be impossible to observe, however. The oscillations had a period ranging from approximately 1.5 to 20 min; the latter could possibly be detected (although damped by diffusion), if sampled at maximum frequency (3 min between each sampling). It appears unproblematic to calculate  $O_2$  in the liquid phase from measured  $O_2$  transport from the headspace (Fig. 5). Refinements of the calculation of  $[O_2]$  are of course possible, by explicit modelling of respiration and transport.

The determination of  $N_2$  production (and mass balance) is unproblematic, thus circumventing the need for  $^{15}\text{N}$  tracer techniques or  $N_2O$  reductase inhibition (acetylene). The detection limit for  $N_2$  production is rather high compared to that for NO and  $N_2O$ , however ( $200 \text{ nmol flask}^{-1} \text{ h}^{-1}$ ), as illustrated in the insert of Fig. 6.

The frequency of sampling is a bottleneck of the system. Each analysis takes 200 s, thus the frequency of sampling cannot exceed  $1 \text{ h}^{-1}$  if 15 cultures (plus three unstirred blanks) are run in parallel. When screening different cultures, which may deplete  $O_2$  at different rates, it would be desirable to allow

the frequency of sampling from each flask to be determined by its O<sub>2</sub> level (increasing the frequency as O<sub>2</sub> is being depleted). This is feasible with the present system, but has not yet been programmed. Similarly, it is possible to program the injection system to provide frequent doses of O<sub>2</sub> (or any other gas) to the flasks, thus programming individual concentrations to be sustained over a period of time.

The system is also suited for measuring oxidation of methane, and any other gas which can be quantified by the GC. It may also be used to study the effect of NO on the metabolism of bacteria, which will require monitoring of NO concentrations due to its instability. NO appears to play an important role in microbial interactions, both in the environment and in the gut, as well as being one of the antimicrobial agents of macrophages (Spiro, 2007).

It is possible to quantify Ne with the present setup of the GC, and this can be used as a tracer for dilution (if spiked to much higher levels than its ambient concentration of 18 ppmv). It would also be desirable to mount a pressure sensor behind the sampling needle, to enable the computer to regulate the pressure (via control of the peristaltic pump).

In principle, the 15 cultures could be run as continuous cultures. Continuous culture is often preferred for studies of regulation, since it is better suited for altering one variable at a time (keeping all other conditions constant). However, batch cultures are suitable for a number of experiments with denitrifying bacteria, if designed properly. One obvious prerequisite is that the initial O<sub>2</sub> concentration should be low enough to ensure depletion long before the batch cultures approach their stationary phase (by depleting other resources than O<sub>2</sub>).

To our knowledge, there exist no other commercial or custom-made instruments that can match our robot regarding high throughput and richness of the datasets for the kinetics of denitrification. In our lab, the robot has provided uniquely refined data for several denitrifying bacteria under a variety of conditions (manuscripts in preparation). We are also using it for comparative studies of culture collections of denitrifying bacteria regarding their response to oxygen, their consecutive or concomitant expression of the three reductase genes (*nir*, *nor*, *nos*), the NO concentrations sustained during active denitrification, and the reduction of N<sub>2</sub>O to N<sub>2</sub>. Previous comparative studies of denitrifying communities (Holtan-Hartwig et al., 2002) were done with a more conventional gas chromatographic approach, lacking the ability to monitor O<sub>2</sub> and NO, and required the use of acetylene inhibition of nitrous oxide reductase to assess the production of N<sub>2</sub>. The present system opens up for much more refined comparative studies of denitrifying communities, to enhance our understanding of the biological component in regulating the emission of NO and N<sub>2</sub>O to the atmosphere.

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